

# DIFFUSION

---

**Bruce E. Logan**

**Department of Civil & Environmental Engineering  
The Pennsylvania State University**

**Email: [blogan@psu.edu](mailto:blogan@psu.edu)**

**<http://www.engr.psu.edu/ce/enve/logan.htm>**

# What are the mechanisms for chemical motion?

---

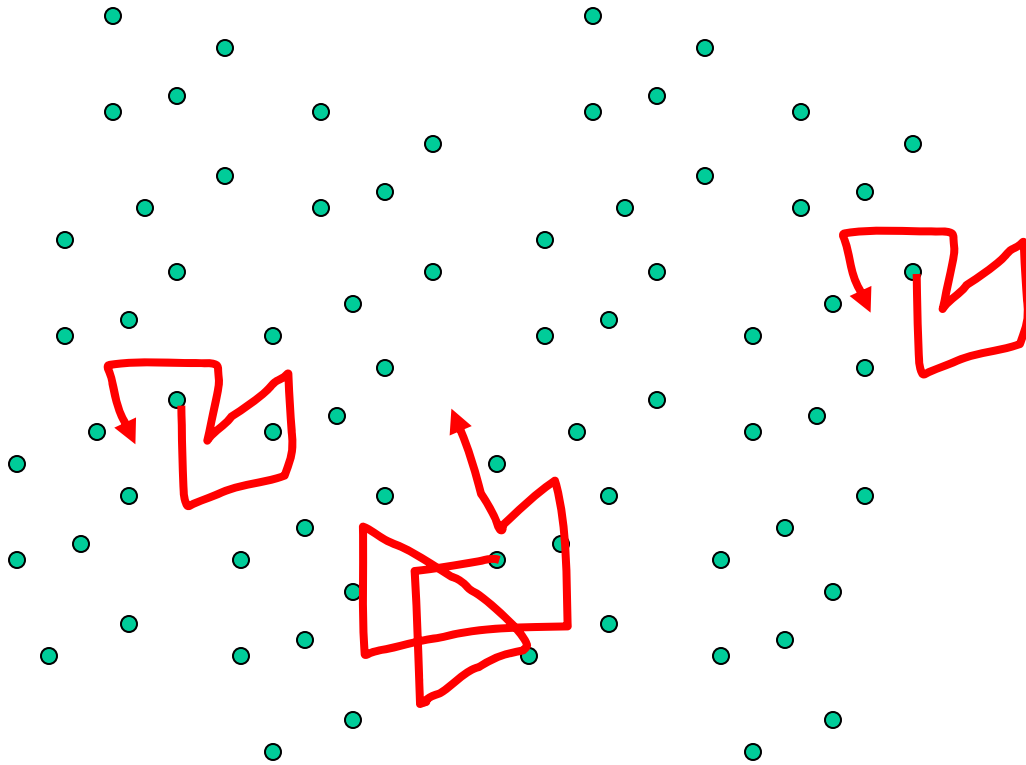
- Advection
  - Bulk transport by imposed flow. Examples: current in a stream, flow in a pipe.
- Convection
  - Transport due to fluid instability. Examples: air rising over a hot road.
- Diffusion- molecular
  - Scattering of particles (molecules) by random motion due to thermal energy
- Diffusion- turbulent
  - Scattering due to fluid turbulence. Also called eddy diffusion. This type of “diffusion” is much faster than molecular diffusion

# Diffusion & Dispersion

---

- Diffusion is a method by which a chemical is dispersed.
- Dispersion is the “spreading out” of a chemical that can be caused by different mechanisms
- Don’t confuse a molecular diffusion coefficient with a dispersion coefficient (more on dispersion will come later in the course).

# Chemical Flux

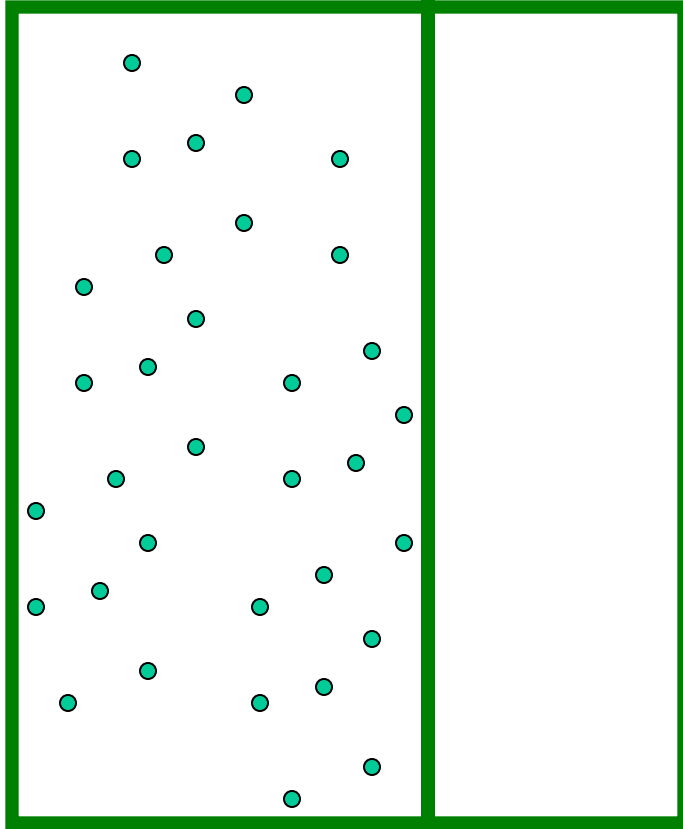


Molecules move in a random direction based on thermal energy

Is there a net flux?

$$\text{Flux} \equiv \frac{\text{Total flow rate}}{\text{Area}} \quad \left[ \frac{\text{moles}}{L^2 - t} \right]$$

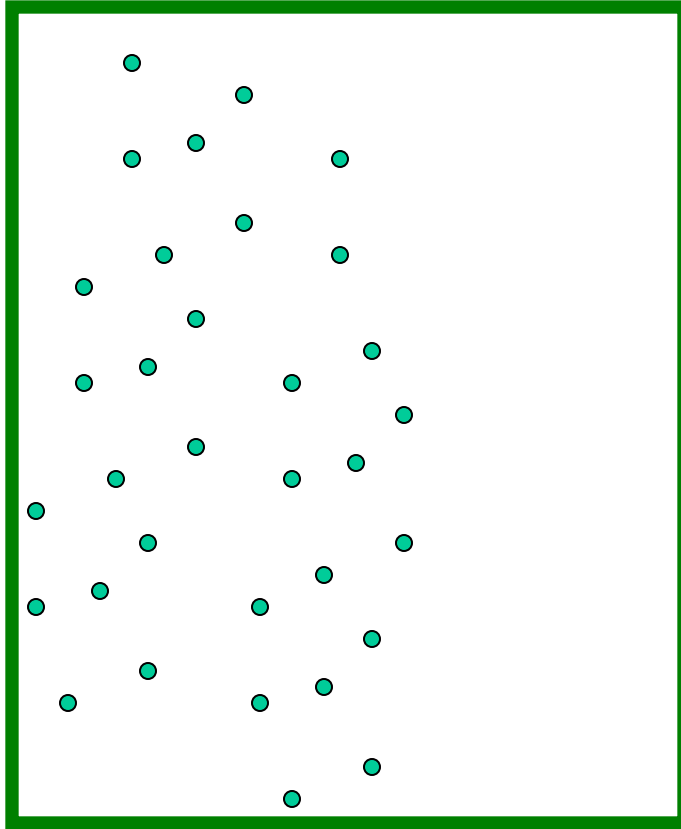
# Chemical Flux



Net flux occurs when molecules move in a direction where there are no molecules to balance their motion back in the opposite direction.

$$\text{Flux} \equiv \frac{\text{Total flow rate}}{\text{Area}} \quad \left[ \frac{\text{moles}}{L^2 - t} \right]$$

# Chemical Flux



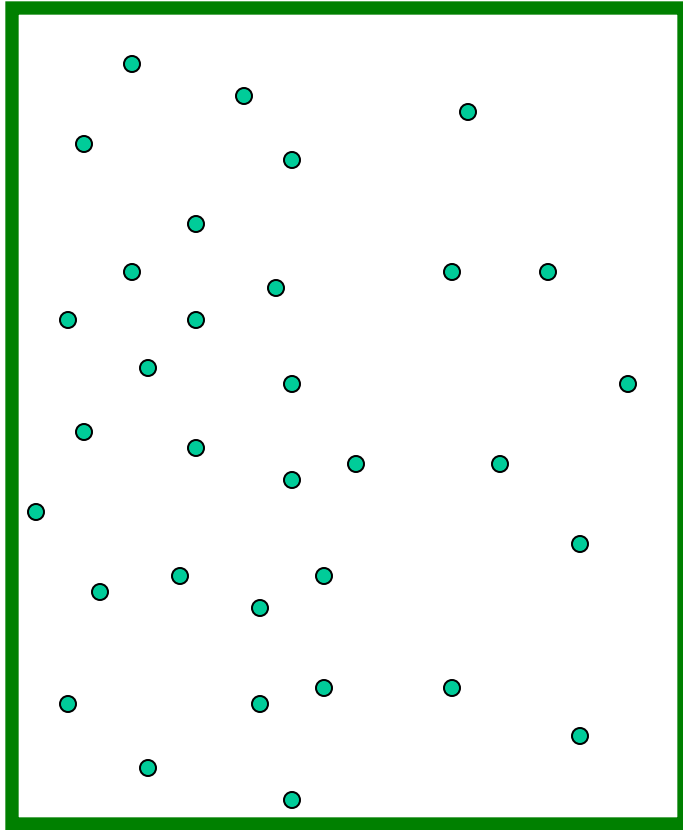
Net flux occurs when molecules move in a direction where there are no molecules to balance their motion back in the opposite direction.



Direction of net chemical flux

$$\text{Flux} \equiv \frac{\text{Total flow rate}}{\text{Area}} \quad \left[ \frac{\text{moles}}{L^2 - t} \right]$$

# Chemical Flux



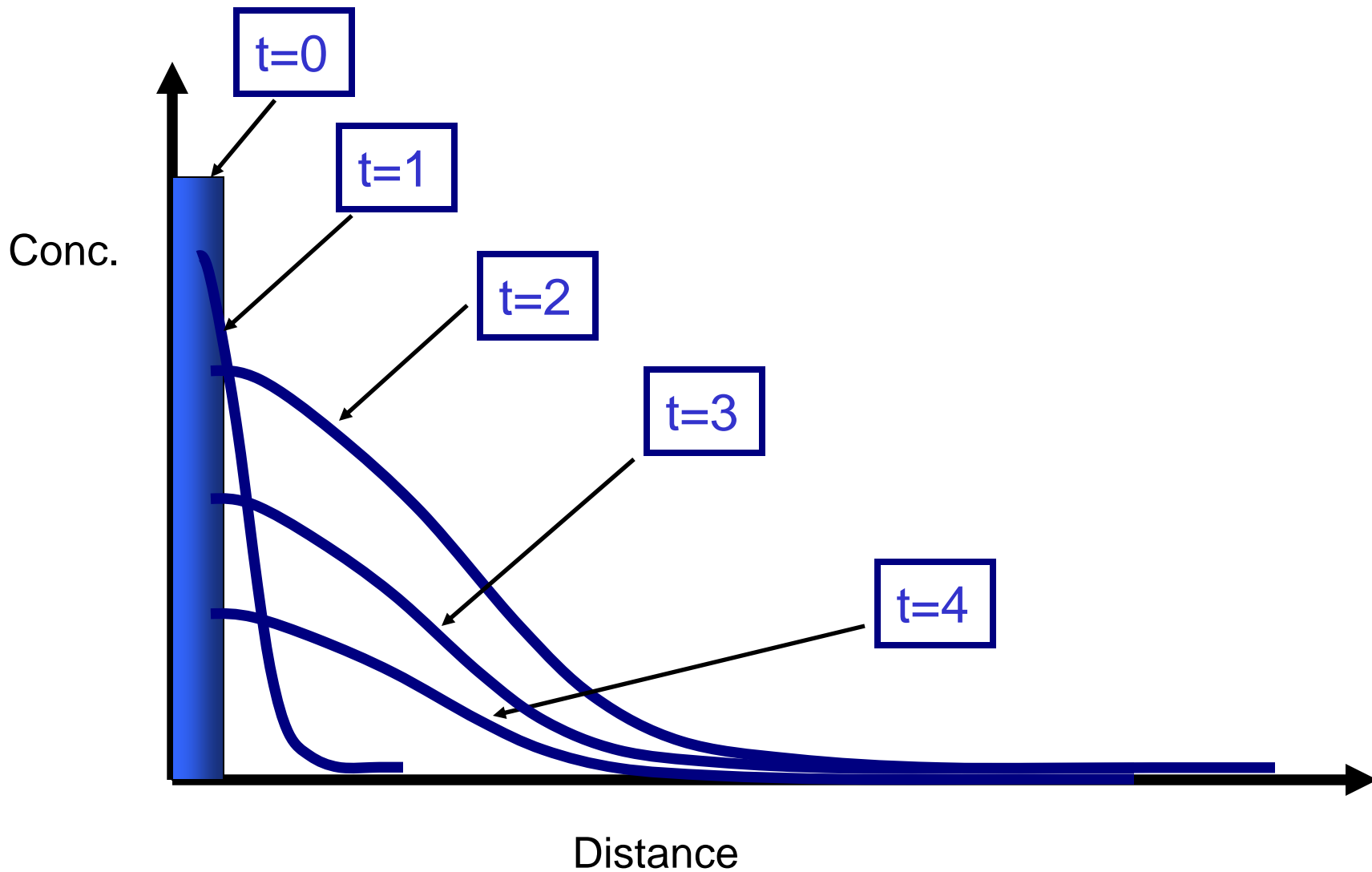
Net flux occurs when molecules move in a direction where there are no molecules to balance their motion back in the opposite direction.



Direction of net chemical flux

$$\text{Flux} \equiv \frac{\text{Total flow rate}}{\text{Area}} \quad \left[ \frac{\text{moles}}{L^2 - t} \right]$$

We often show chemical flux graphically as concentration versus time





# Fick's First Law

Fick recognized that there must be a difference in concentration to drive the net diffusion of a chemical, and formulated the law:

$$j_{Cw,z} = -c_w D_{Cw} \frac{dx_C}{dz}$$

$c_w$  = molar density of water

$dx_C/dz$  = molar gradient of C in z-direction

$j_{Cw,z}$  = molar flux of C in z-direction

$D$  = Diffusion constant (fitted parameter)

# Fick's First Law

Fick recognized that there must be a difference in concentration to drive the net diffusion of a chemical, and formulated the law:

$$j_{Cw,z} = -c_w D_{Cw} \frac{dx_c}{dz}$$

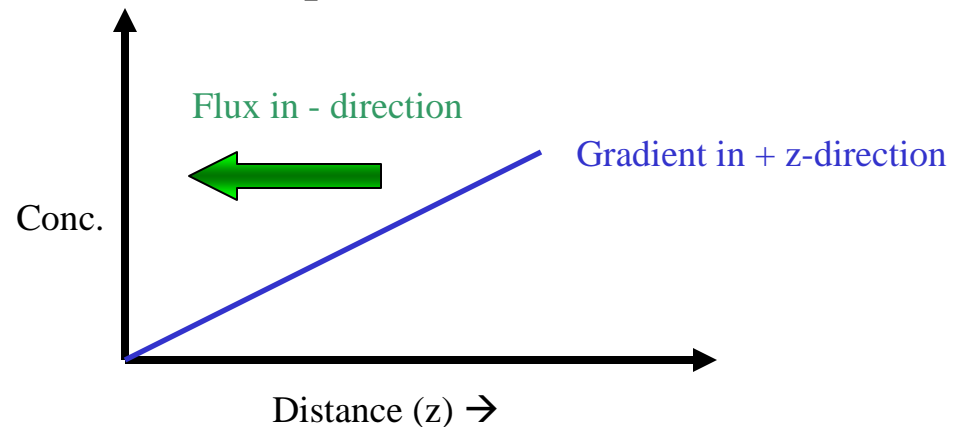
Note negative sign  
(flux in direction  
opposite to gradient)

$c_w$  = molar density of water

$dx_c/dz$  = molar gradient of C in z-direction

$j_{Cw,z}$  = molar flux of C in z-direction

$D$  = Diffusion constant (fitted parameter)



# Fick's First Law

Fick recognized that there must be a difference in concentration to drive the net diffusion of a chemical, and formulated the law:

$$j_{Cw,z} = -c_w D_{Cw} \frac{dx_C}{dz}$$

$c_w$  = molar density of water

$dx_C/dz$  = molar gradient of C in z-direction

$j_{Cw,z}$  = molar flux of C in z-direction

$D$  = Diffusion constant (fitted parameter)

Under isothermal, isobaric conditions, this can be simplified to:

$$j_{Cw,z} = -D_{Cw} \frac{dc_{Cw}}{dz}$$

## Flux in different directions:

$$j_{Cw,x} = -c_w D_{Cw} \frac{dx_C}{dx}$$

$$j_{Cw,y} = -c_w D_{Cw} \frac{dx_C}{dy}$$

$$j_{Cw,z} = -c_w D_{Cw} \frac{dx_C}{dz}$$

$$j_{Cw,r} = -c_w D_{Cw} \frac{dx_C}{dr}$$

# Typical values of Diffusion Coefficient

Gas	$D_{Ca} = 10^{-1} \text{ [cm}^2\text{/s]}$
Liquid	$D_{Cw} = 10^{-5} \text{ [cm}^2\text{/s]}$
Solid	$D_{Cw} = 10^{-10} \text{ [cm}^2\text{/s]}$

# EXAMPLE CALCULATION

- A jar of phenol contaminates a room with only one cylindrical vent (10 cm diameter, 20 cm deep)
- Neglecting advection, what is the rate of phenol loss through the vent if the room concentration of phenol in air is 0.05%?
- Assume: constant temperature of 20°C; a linear concentration gradient in the vent;  $D_{pa}=10^{-1} \text{ cm}^2/\text{s}$ .

## Solution...

$$j_{Pa,z} = -c_a D_{Pa} \frac{dy_C}{dz} = -D_{Pa} \frac{dc_{Pa}}{dz} \approx -D_{Pa} \frac{\Delta c_{Pa}}{\Delta z} = -D_{Pa} \frac{(c_{Pa,1} - 0)}{(0 - z_2)}$$

$$\text{Rate: } W_{Pa,z} = j_{Pa,z} A = \frac{D_{Pa} c_{Pa,1} A}{z_2}$$

$$c_{Pa,1} = y_P c_a = (0.0005) \left( \frac{\text{mole}}{24.1 \text{ L}} \right) = 2.1 \times 10^{-5} \frac{\text{mol}}{\text{L}}$$

$$A = \frac{\pi}{4} d^2 = \frac{\pi}{4} (10 \text{ cm})^2 = 79 \text{ cm}^2$$

$$W_{Pa,z} = \frac{(10^{-1} \text{ cm}^2 / \text{s})(2.1 \times 10^{-5} \text{ mol} / \text{L})(79 \text{ cm}^2) 10^{-3} \text{ L}}{(20 \text{ cm}) \text{ cm}^3}$$

$$W_{Pa,z} = 8.2 \times 10^{-9} \text{ mol/s}$$

# Fick's Second Law

What is the effect of time on the flux? Or... how does the flux change over time?

$$\frac{\text{change in conc}}{\Delta t} \propto \frac{\Delta \text{conc. gradient}}{\Delta \text{ distance}}$$

$$\frac{\Delta c}{\Delta t} = D \frac{\Delta(\Delta c / \Delta z)}{\Delta z}$$

$$\frac{\partial c}{\partial t} = D \frac{\partial(\partial c / \partial z)}{\partial z} = D \frac{\partial^2 c}{\partial z^2}$$



# Fick's Second Law

For a chemical in water:

$$\frac{\partial c_{Cw}}{\partial t} = D_{Cw} \frac{\partial^2 c_{Cw}}{\partial z^2}$$

At steady state,

$$\frac{\partial c_{Cw}}{\partial t} = 0$$

so this becomes

$$\frac{\partial c_{Cw}}{\partial t} = 0 = D_{Cw} \frac{\partial^2 c_{Cw}}{\partial z^2}$$

and we have that

$$\frac{dc_{Cw}}{dz} = \text{constant}$$

This tells us that at steady state, the flux is constant, i.e.

$$j_{Cw,x} = -c_w D_{Cw} \frac{dx_c}{dx}$$

Fick's  
First Law

# How to calculate Diffusion Coefficients?

---

- General Approaches
  - Tabulated values- best approach
  - Correlations- many can exist
  - Experimental- can be time consuming
- Air Correlations for  $D_{Ca}$ 
  - Kinetic theory of gases: many limitations, such as binary mixture.
  - Hirshfelder correlation: requires a lot of constants
  - Fuller correlation: best approach

# FULLER CORRELATION: Diffusivities from Structure

---

## Chemical “C” in gas “g”

Where: [these units must be used]

$D_{Ca}$  = diffusion coefficient [cm<sup>2</sup>/s]

T = temperature [K]

P = pressure [atm]

$M_C$  = molecular weight of chemical [g/mol]

$M_g$  = molecular weight of gas [g/mol]

$V_{C,d}$  = atomic diffusion volume (from formula and tabulated values) [cm<sup>3</sup>]

$$D_{Cg} = \frac{T^{1.75} \times 10^{-3}}{P (V_{C,d}^{1/3} + V_{g,d}^{1/3})^2} \left( \frac{1}{M_C} + \frac{1}{M_g} \right)^{1/2}$$

For chemicals

in air:



$$D_{Ca} = \frac{T^{1.75} \times 10^{-3}}{P (V_{C,d}^{1/3} + 2.73)^2} \left( \frac{1}{M_C} + 0.0345 \right)^{1/2}$$

**TABLE 3.1 Atomic Diffusion Volumes for Use in Estimating  $D_{Cs}$  by Method of Fuller et al.**

Atomic and Structure Diffusion–Volume Increments, $v$					
C	16.5	Cl	19.5		
H	1.98	S	17.0		
O	5.48	Aromatic ring	–20.2		
N	5.69	Heterocyclic ring	–20.2		
Diffusion Volumes for Simple Molecules, $v$					
H <sub>2</sub>	7.07	Ar	16.1	H <sub>2</sub> O	12.7
D <sub>2</sub>	6.70	Kr	22.8	CClF <sub>2</sub>	114.8
He	2.88	CO	18.9	SF <sub>6</sub>	69.7
N <sub>2</sub>	17.9	CO <sub>2</sub>	26.9	Cl <sub>2</sub>	37.7
O <sub>2</sub>	16.6	N <sub>2</sub> O	35.9	Br <sub>2</sub>	41.1
Air	20.1	NH <sub>3</sub>	14.9	SO <sub>2</sub>	41.1

Source: Welty et al., 1984.

# How to calculate Diffusion Coefficients?

---

- Water: more on this later
- Solids
  - Less information available
  - Chemical in porous medium is in liquid phase: hindered diffusion
  - Chemical adsorbed to soil is in “solid” phase: surface diffusion
  - For hindered and surface diffusion, need to know diffusion constant in water

# Examples: Diffusion constants in/on solids

## Hindered diffusion

$$D_{Cw,pm} = D_{Cw,h} \frac{\theta}{\tau}$$

Where:

$D_{Cw,pm}$  = diffusion coefficient in porous medium

$D_{Cw,h}$  = diffusion coefficient in a single pore

$\theta$  = porosity; typically 0.3

$\tau$  = tortuosity factor; typically 3

## Surface diffusion

$$D_{Cw,h+sur} = D_{Cw,h} + \frac{(1-\theta)K^* D_{Cw,sur}}{\theta}$$

Where:

$D_{Cw,h+sur}$  = overall surface diffusion coefficient

$D_{Cw,sur}$  = surface diffusion coefficient

$K^*$  = dimensionless adsorption partition coefficient

# Diffusion constants: summary

---

- Tabulated values always best
- For air, simple correlations should be sufficient for level of our calculations
- In a porous medium, porosity and tortuosity factors probably more important than correct value for molecular diffusion in air.
- For water, situation is much more complex... more on that next.